



**MARY KAY O'CONNOR
PROCESS SAFETY CENTER**
TEXAS A&M ENGINEERING EXPERIMENT STATION

LNG Safety Excellence: A Decade of Efforts by the Mary Kay O'Connor Process Safety Center

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Artie McFerrin Department of

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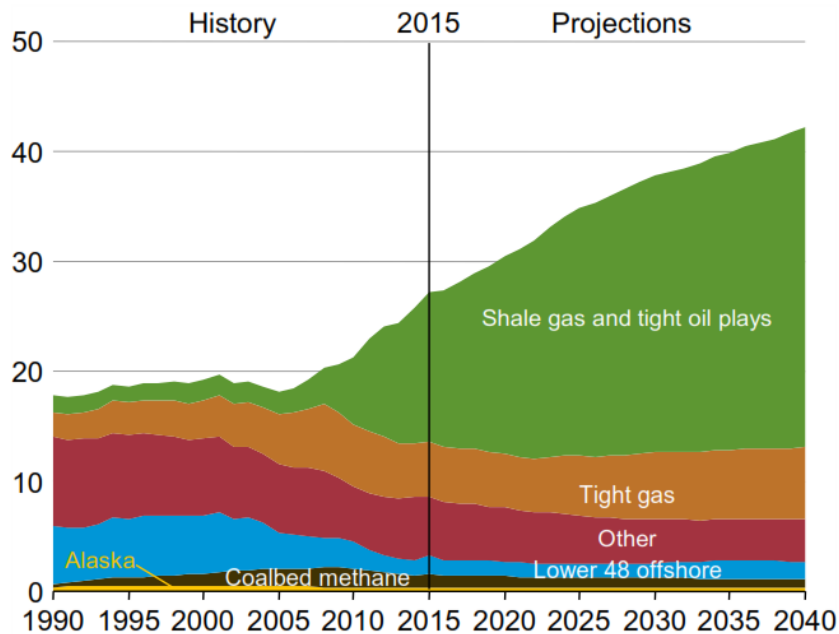
Outline

- Introduction
- LNG Safety Concerns
- LNG Safety Research Overview
- Areas of Study
 - LNG Vapor Dispersion and Pool Fire Modeling with CFD
 - LNG Vapor Cloud Control using Water Curtain
 - LNG Vapor and Fire Mitigation using Expansion Foam
 - Experimental Study and CFD Simulation of Bund Overtopping
 - Source-Term and Pool Spreading of Spill on Land and Water
- Conclusions

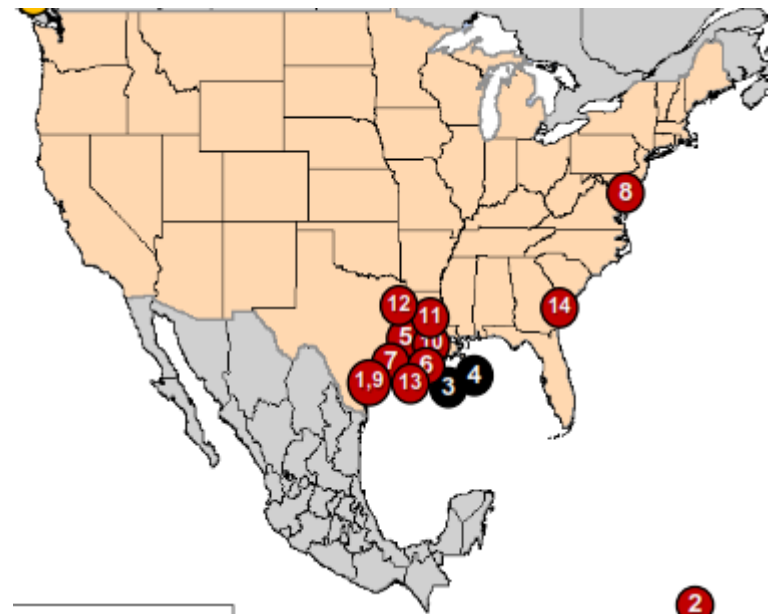


Introduction

- Liquefied natural gas (LNG): provides flexibility in natural gas industry for storage and inter-regional trade
 - New emerging natural gas market will accelerate LNG trade globally
- Growing concerns on potential LNG spill and consequence around facilities
 - Further research on LNG safety is required to ensure public safety and safe operation



U.S. natural gas production by source (trillion cubic feet) (source: EIA)



LNG import and export terminals approved in the U.S. (source: FERC)



LNG Safety Concerns

LNG Properties

- Flammable as a fuel
 - Flammable limit ranges approximately 5-15 v/v % in air
- Cryogenic liquid for ease of storage and transportation
 - Extremely cold, boiling point is -162°C (-263°F)
 - Expands 600 times in volume during vaporization
 - Difficult to disperse due to heavier-than-air behavior below -114°C (-173°F)

Hazards and Regulations

- Main hazards
 - ❑ Flammable vapor cloud
 - ❑ Pool fire
- Standards and regulations
 - ❑ 49 CFR Part 193
 - Define “exclusion zones” in terms of vapor dispersion (1/2 LFL) and fire thermal radiation (5 kW/m^2)
 - ❑ NFPA 59A (2013)
 - Require mitigation measures to reduce risks to a tolerable level



LNG Safety Research at MKOPSC

- Involved in research for the improvements of LNG safety, security and spill response since 2005
- Research program, sponsored by **BP Global Gas SPU, Qatar National Research Foundation**, and **others** includes
 - LNG vapor dispersion and pool fire
 - LNG vapor dispersion and pool fire CFD modeling and validation
 - Safety measures for dispersion and fire control
 - Application of water curtain to disperse LNG vapor cloud
 - Application of expansion foam and alternate systems to control LNG vapor and fire
 - Risk analysis of bund overtopping
 - Source-term and pool spreading of spill on land and water
- Combination of theoretical understanding with field/lab tests to make the research applicable to the current industry needs





LNG Facility at TEEEX

- Seven series of LNG outdoor spill tests have been performed since 2005 at LNG test facility at the Brayton Fire Training Field (BFTF) of Texas A&M Engineering Extension Service (TEEX), College Station, Texas



- Pit 1: Small Pit - 3m x 3m x 1.22 m
- Pit 2: Large Pit - 10m x 6.7m x 1.22m
- Pit 3: L-shaped trench
- Pit 4: Marine Pit - 2.44 m x 6.7 m x 6.7 m

- Average total vol. of LNG used: 41 m³
- Average spill rate: 0.36 ~ 1 m³/min
- Data measured
 - Wind speed, direction, temperature, humidity, atmospheric heat flux
 - LNG flow, level, temperature
 - LNG vapor turbulence, speed, concentration, temperature
 - LNG fire temperature, heat flux

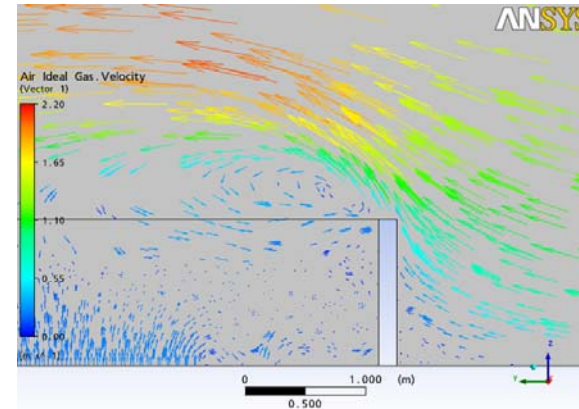
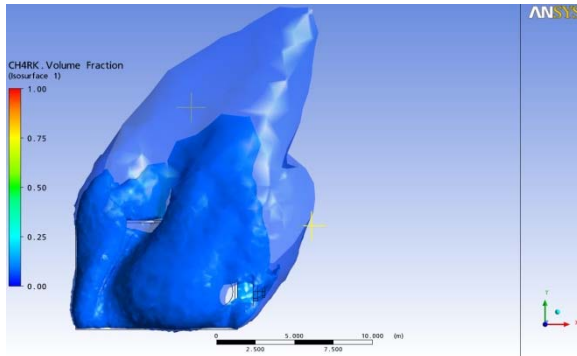


LNG Vapor Dispersion and Pool Fire Modeling with CFD



LNG Vapor Dispersion and Pool Fire

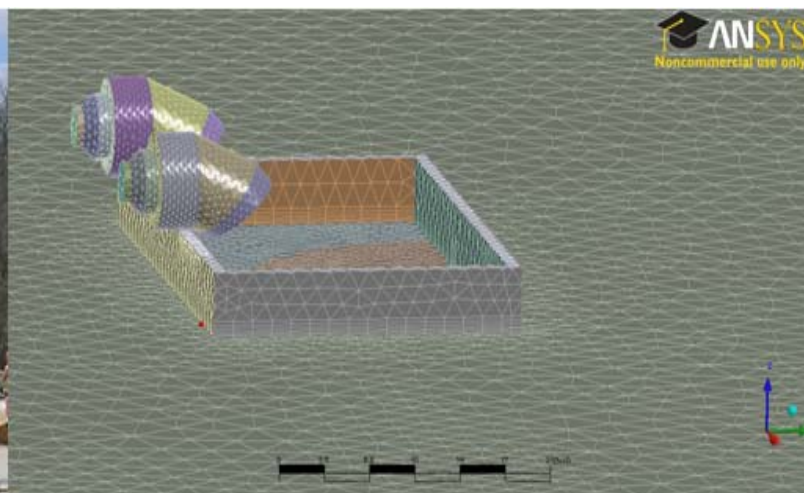
- High demand exists for performing site-specific risk analysis of complex scenarios in LNG facilities and terminals
- No specific guideline on how to address complex scenarios with CFD
- Improve the understanding of physical process of LNG vapor dispersion and pool fire
- Study key parameters of modeling LNG vapor dispersion and pool fire with CFD codes





LNG Vapor Dispersion and Pool Fire

- **Field test setup**



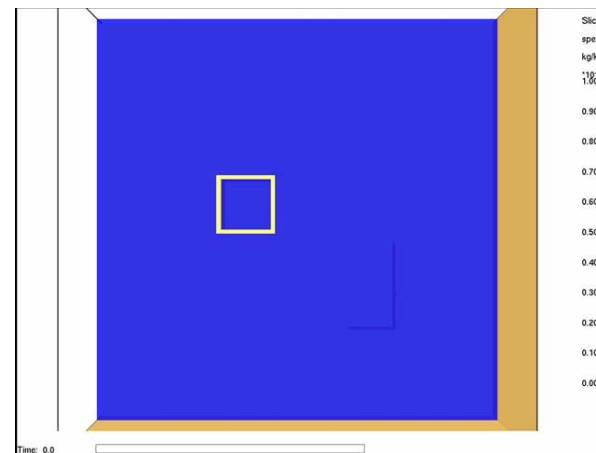
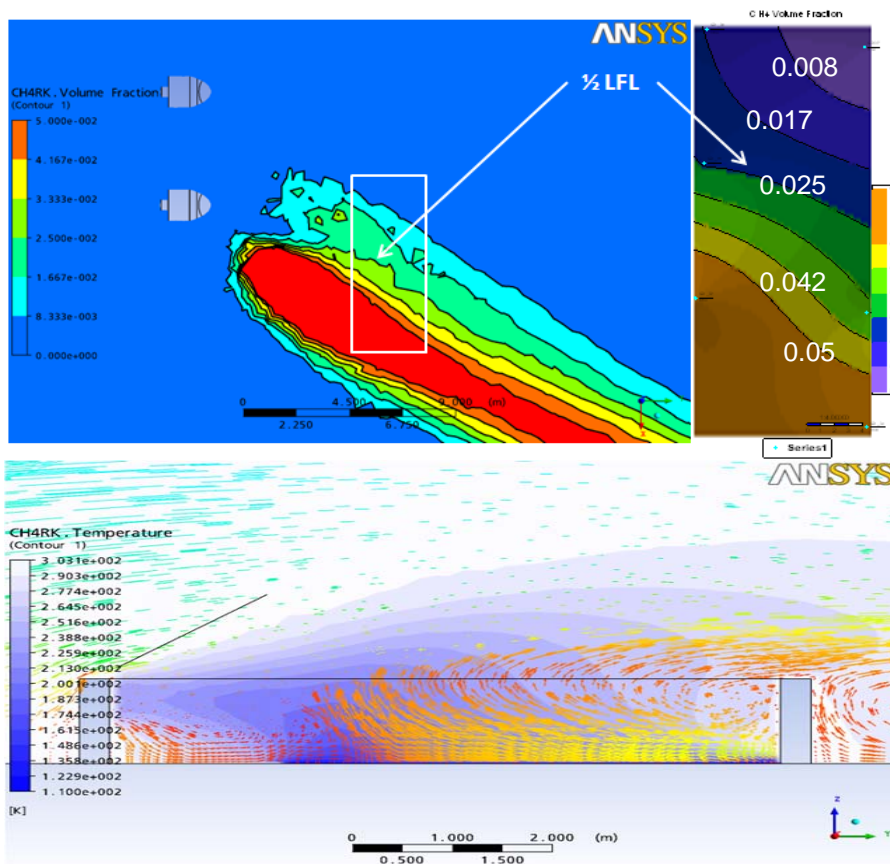


LNG Vapor Dispersion and Pool Fire





LNG Vapor Dispersion and Pool Fire



Comparison of gas concentration contours and effect of turbulence induced by the dike

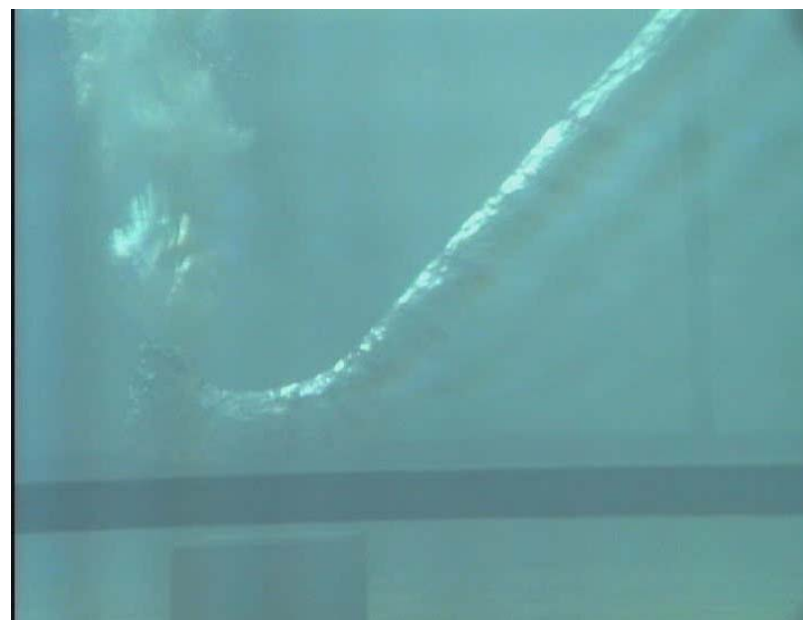


LNG Vapor Dispersion and Pool Fire

- LNG underwater release



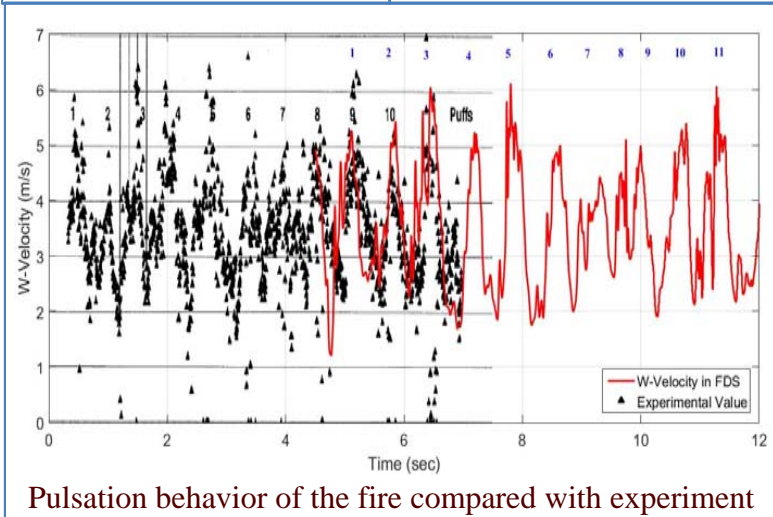
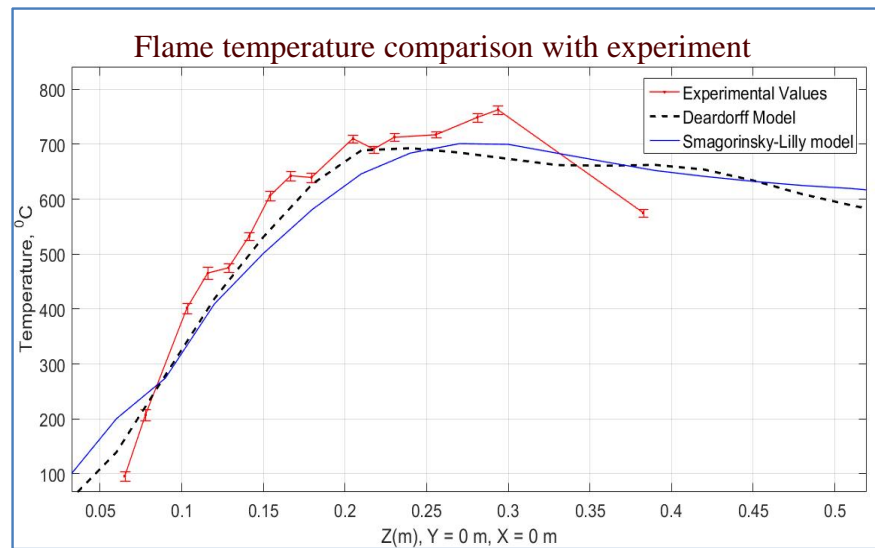
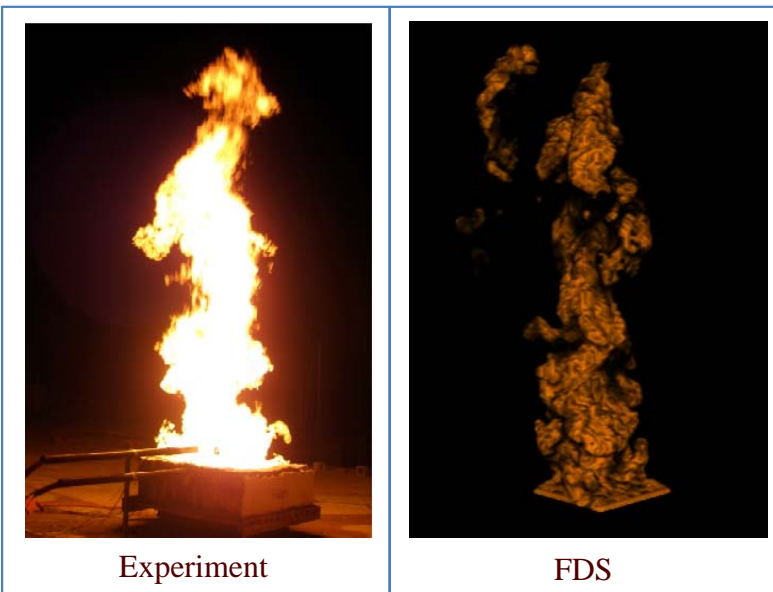
Over-the-land video camera



Underwater video camera



LNG Vapor Dispersion and Pool Fire



R3 (-2, -2, 0.9) m R4 (-2.2, -0.1, 0.9) m

Source	R3 (kW/m ²)	R4 (kW/m ²)
Experiment	2.5	5.0
FDS-Deardorff	3.1 (+22%)	5.5 (+11%)
FDS-Smagorinsky	3.5 (+39%)	6.4 (+28%)

Deardorff turbulence model results in better accuracy
of radiation prediction





LNG Vapor Cloud Control using Water Curtain



Controlling LNG Vapor Cloud using Water Curtain

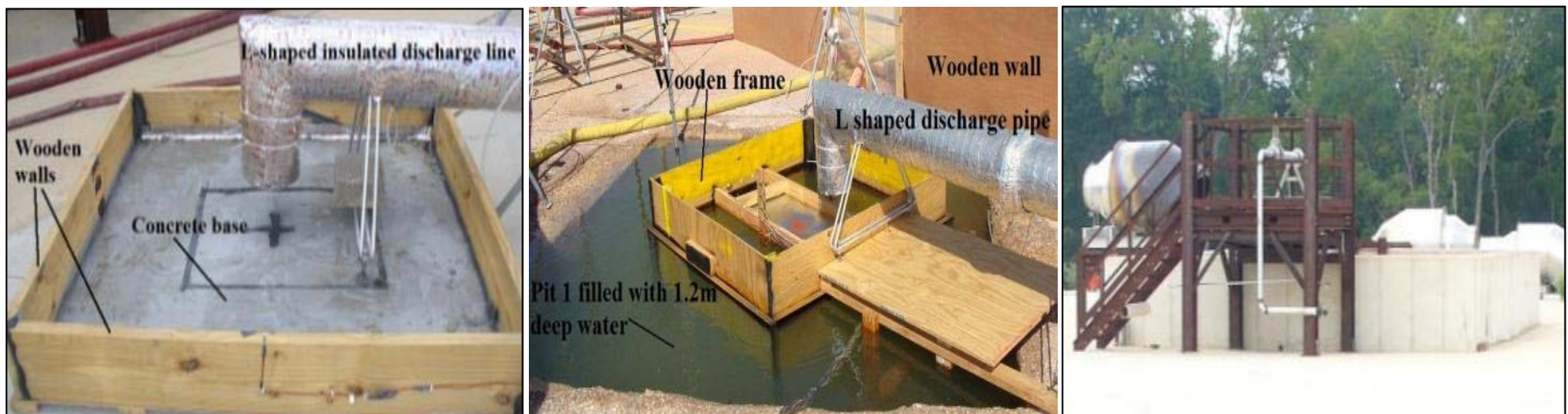
- Water curtain is considered one of the most effective engineering methods in mitigating various types of hazards
- No definitive and comprehensive guideline for water curtain design in LNG vapor control
- Determine the key parametric dependence of different water curtains in controlling the LNG vapor cloud
- Develop an effective engineering guideline for water curtain application





Controlling LNG Vapor Cloud using Water Curtain

Experiment design



□ Facility: Brayton Fire Training Field

Pit 1 (3m x 3m x 1.22m) filled with water up to 1.2m

Wooden confinement (1.52m x 1.52m x 0.31m)

3 types spray: Fan, Conical and Fog



Fan type



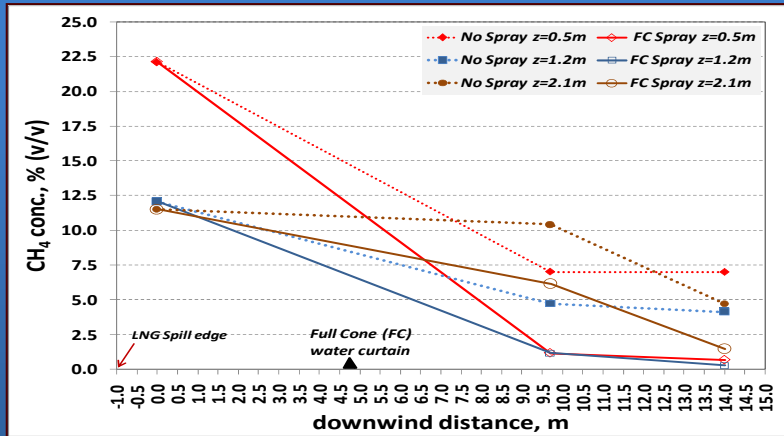
Conical type



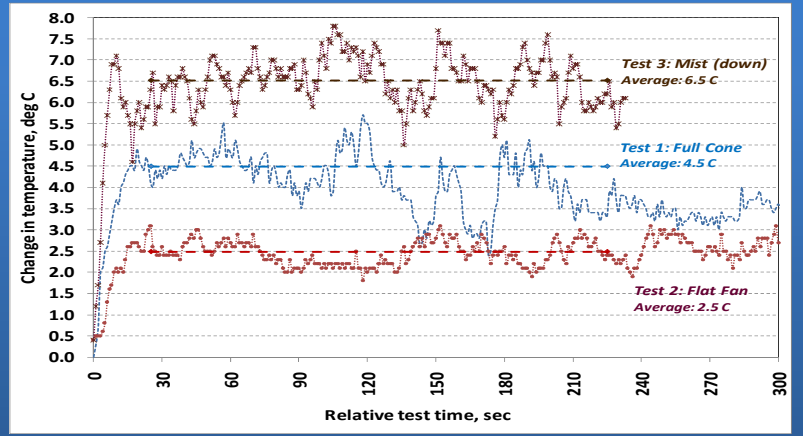
Fog type



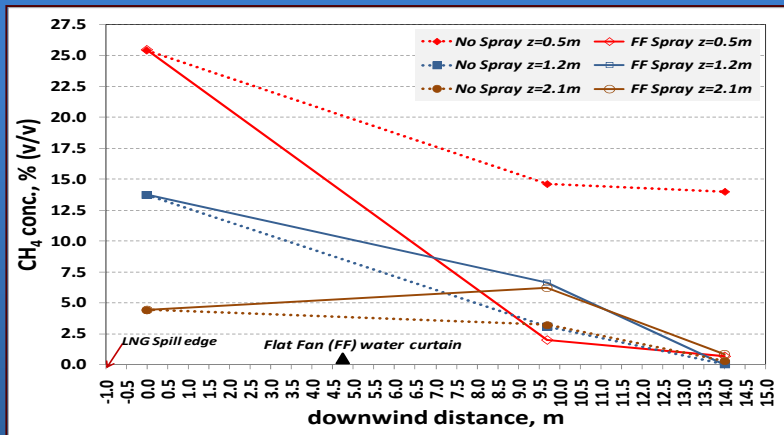
Controlling LNG Vapor Cloud using Water Curtain



Conc. at 3 different height with/wo full cone type



Change in water spray temperature reading



Conc. at 3 different height with/wo flat-fan type

Droplet Size: Mist Cone < Full Cone < Flat Fan
Heat Transfer Rate :

Flat Fan < Full Cone < Mist Cone



1

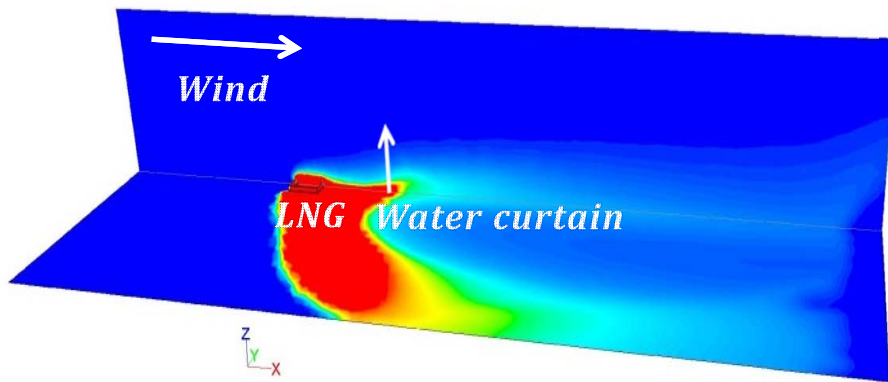
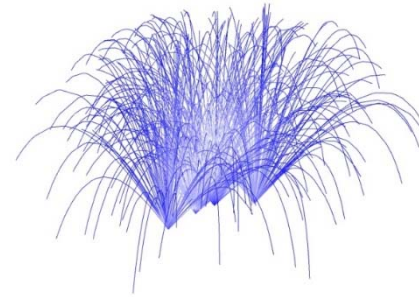
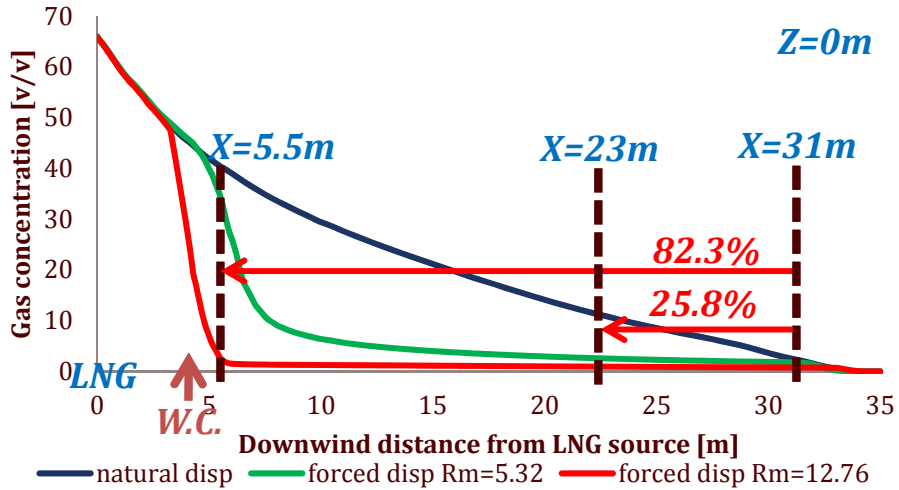
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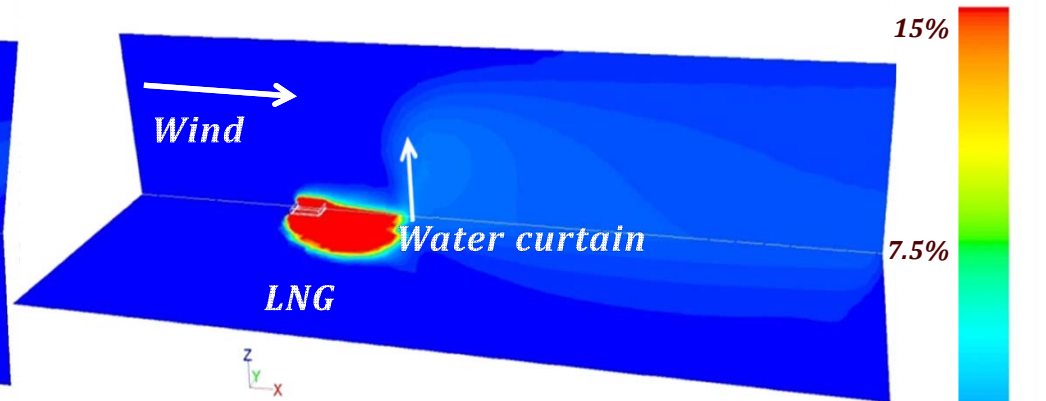


Controlling LNG Vapor Cloud using Water Curtain

- Forced Dispersion at $R_M=5.32$ & 12.76



Forced Dispersion ($t=200s$) ($R_M = 5.32$)



Forced Dispersion ($t=200s$) ($R_M = 12.76$)



LNG Vapor and Fire Mitigation using Expansion Foam



High Expansion Foam

Low expansion

- up to 20

Medium expansion

- 20 to 200

High expansion

- 200 to 1000

NFPA 11: Standard for Low-, Medium-, and High-Expansion Foam

- ❖ Vapor hazard mitigation
- ❖ Pool fire control

- ❖ Study required to understand the physical phenomena and develop specific guidelines for foam system design

Foam= Foam solution+ Air



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LNG Vapor and Fire Mitigation using Foam



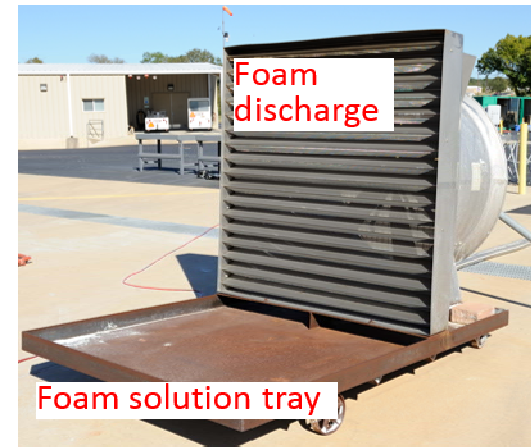
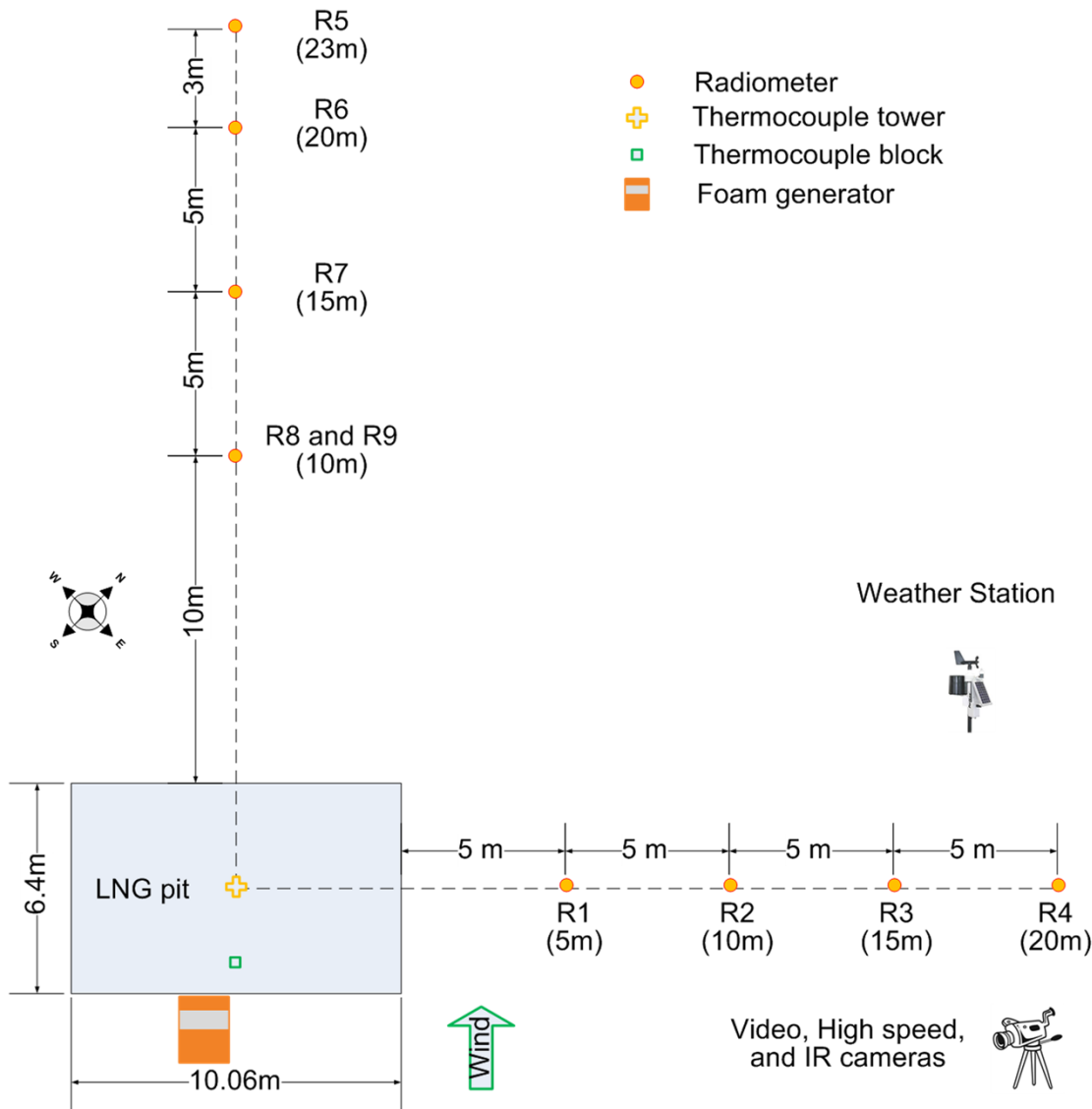


LNG Vapor and Fire Mitigation using Foam



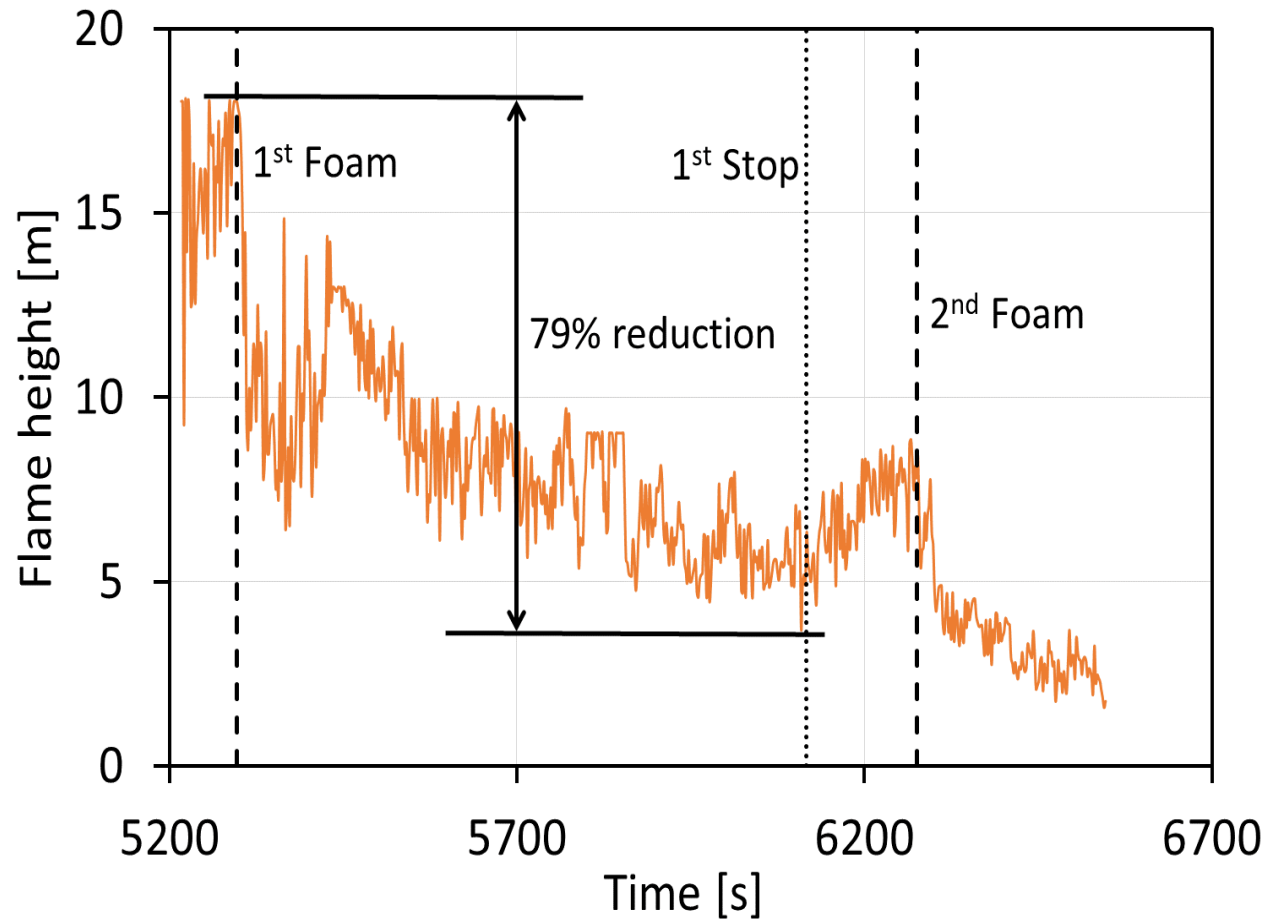


LNG Vapor and Fire Mitigation using Foam





LNG Vapor and Fire Mitigation using Foam



The idea of intermittency $I(L)$ was used to determine average flame length

The average flame length was **16.34 m** for the fire without foam application, which is the flame length with an intermittency of 0.5



Experimental Study and CFD Simulation of Bund Overtopping



Bund Overtopping

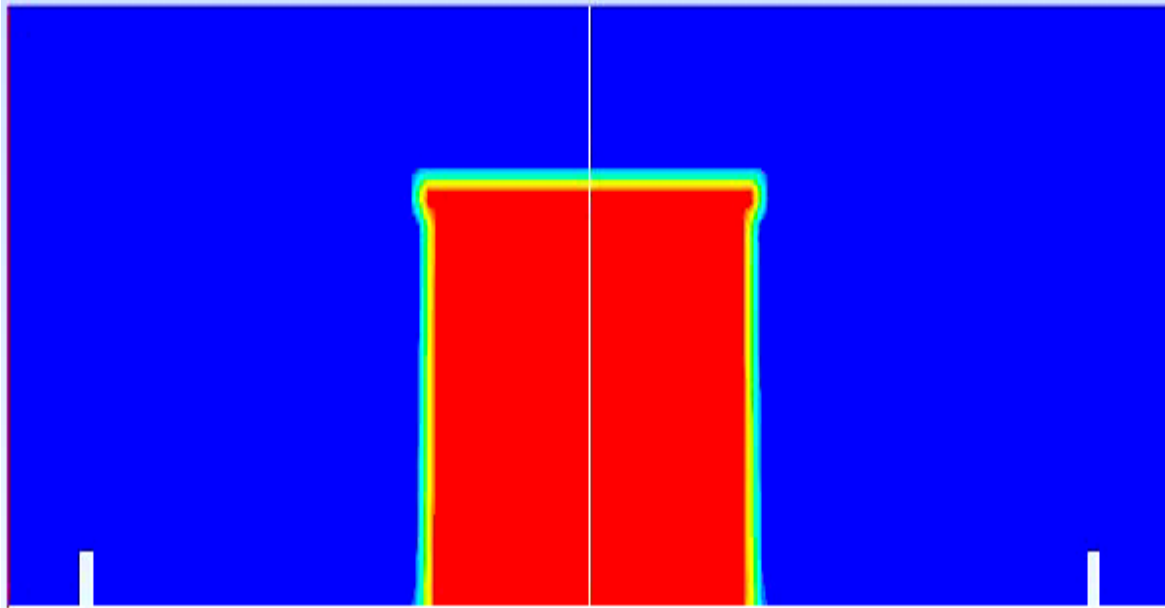
- Roles of Bund
 - Secondary containment
 - Limit contamination
 - Reduce vaporization
 - Control pool fire impact
- Capacity of Bund
 - **$\geq 110\%$ * tank capacity**





Bund Overtopping

Scenario - Catastrophic Tank Failure

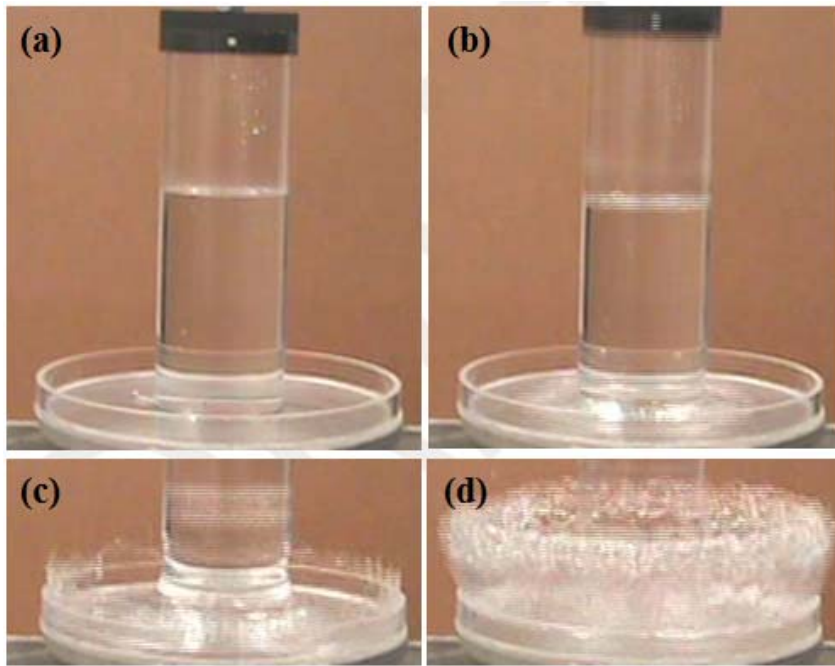


Video – CFD Simulation on [Bund Overtopping](#) in case of catastrophic tank failure.



Bund Overtopping

- Lab test



Snap of the overtopping process: (a) 0.0 s; (b) 0.1 s; (c) 0.2 s; (d) 0.3 s.

- Field test



Setup of bund overtopping test at Brayton Fire Training Field



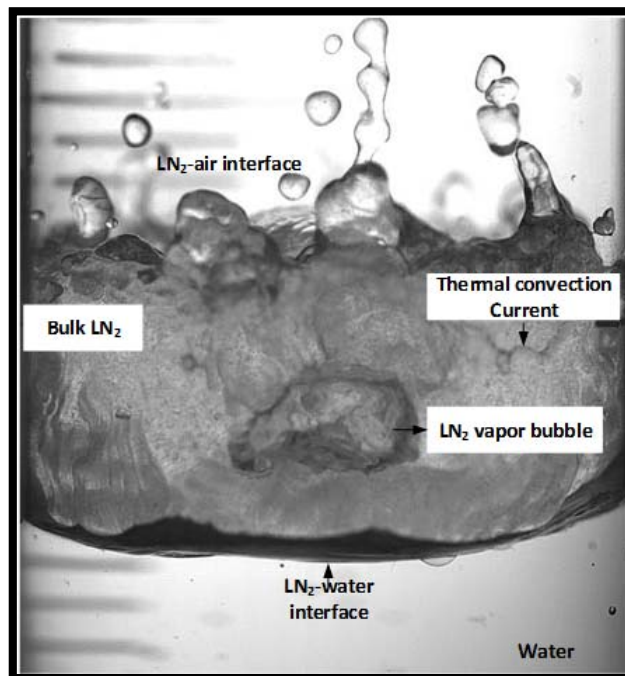
Source-Term and Pool Spreading of Spill on Land and Water



LNG Spill on Water



Experimental setup for release of LN₂ on water



High-speed Image from flow visualization experiment

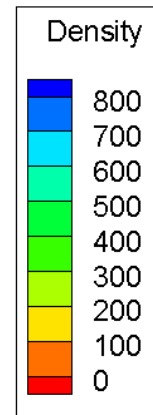
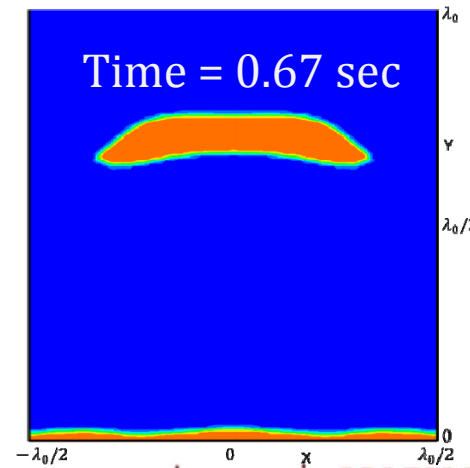
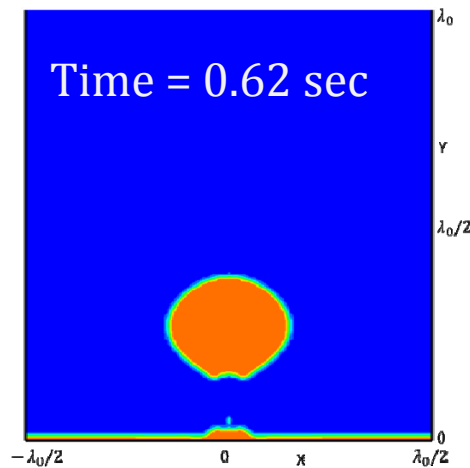
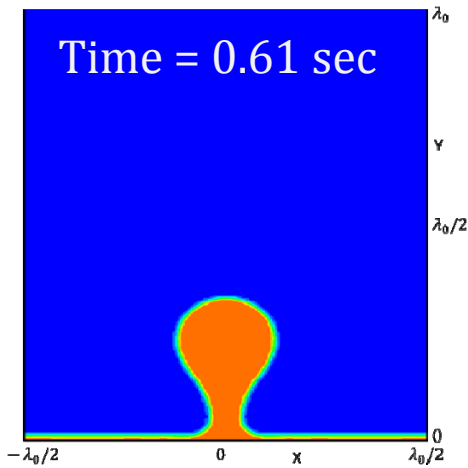
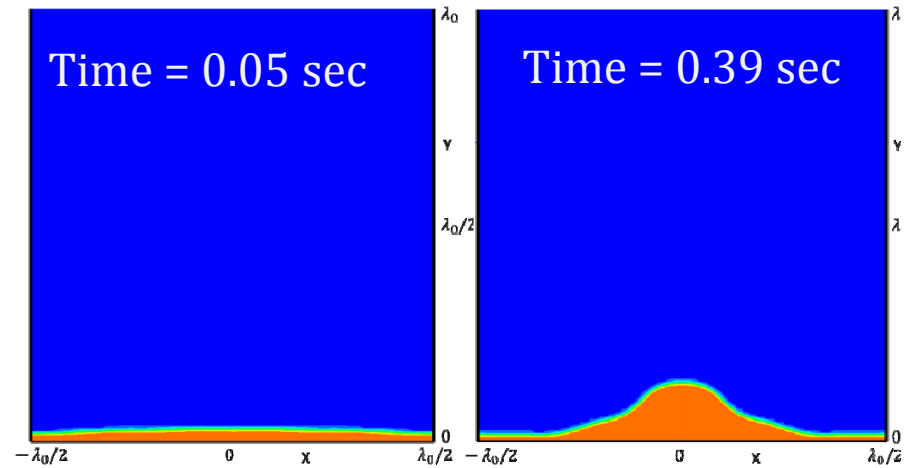
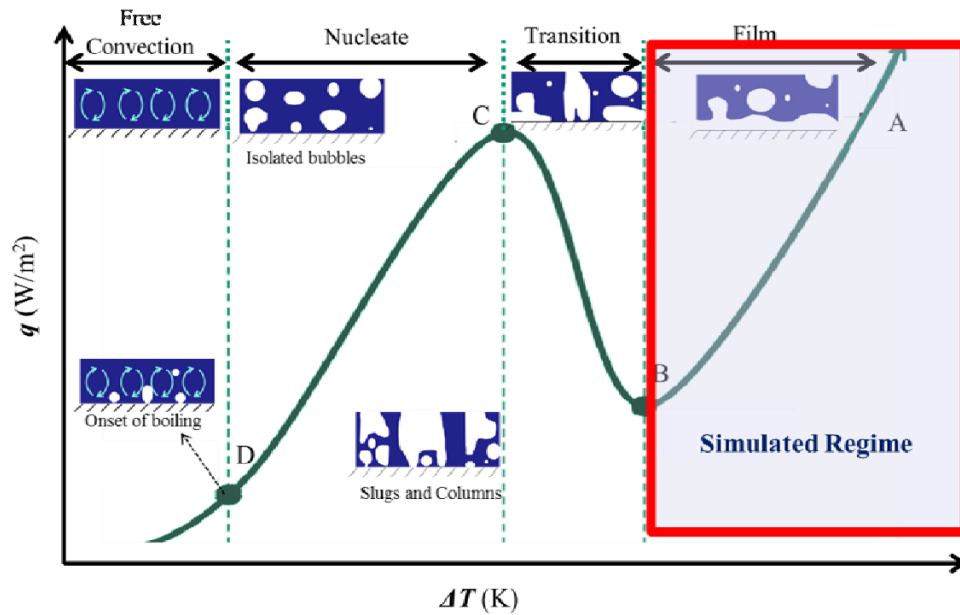


L-Shaped Trench

LNG release in L-Shaped Trench, Release duration – 1200 s



LNG Spill on Land





Publications

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- Gopaldaswami, N., Laboureur, D. M., Mentzer, R. A., & Mannan, M. S. (2016). Quantification of turbulence in cryogenic liquid using high speed flow visualization. *Journal of Loss Prevention in the Process Industries*, 42, 70–81.
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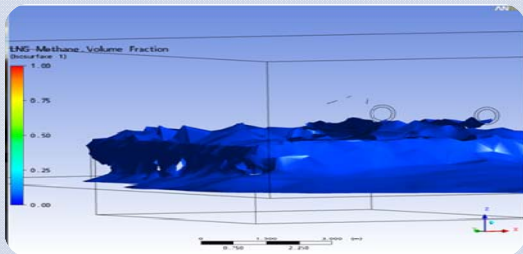


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Conclusions



Understand complex phenomena of LNG vapor dispersion and pool fire



Understand water curtain mechanisms to disperse the LNG cloud



Understand the mitigation effect of foam on LNG vapor and fire scenarios



Assess the risk of LNG overtopping and provide recommendations for dike design



Understand the LNG spill phenomena and develop accurate source term and pool spreading model



Acknowledgements

- Dr. Bin Zhang
- LNG Safety Team of MKOPSC



The background of the slide is a dark red, semi-transparent image of the Texas State Capitol building in Austin. The building's iconic dome is at the top center, and a statue of George Washington is visible in the foreground. The overall tone is formal and academic.

Thank you!

Questions and Comments?



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